

The Nuclearity of the Active Site for Methane to Methanol Conversion in Cu-Mordenite: A Quantitative Assessment

Dimitrios K. Pappas,[†] Andrea Martini,^{‡,§} Michael Dyballa,^{†,||,○} Karoline Kvande,[†] Shewangizaw Teketel,[⊥] Kirill A. Lomachenko,[#] Rafal Baran,[#] Pieter Glatzel,[#] Bjørnar Arstad,^{||} Gloria Berlier,[‡] Carlo Lamberti,^{§,▽} Silvia Bordiga,^{†,‡} Unni Olsbye,[†] Stian Svelle,^{*,†} Pablo Beato,^{*,⊥} and Elisa Borfecchia^{*,‡,⊥}

[†]Center for Materials Science and Nanotechnology, Department of Chemistry, University of Oslo, 1033 Blindern, 0315 Oslo, Norway

[‡]Department of Chemistry and INSTM Reference Center and [▽]Department of Physics, University of Turin, 10125 Turin, Italy

[§]IRC "Smart Materials", Southern Federal University, Zorge Street 5, 344090 Rostov-on-Don, Russia

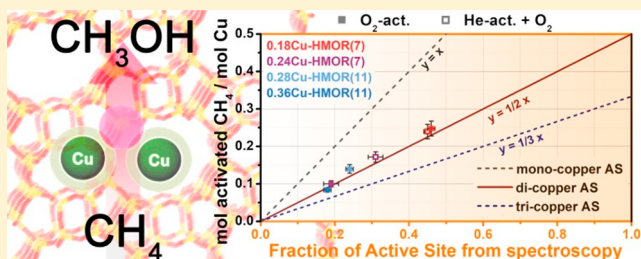
^{||}SINTEF Industry, Forskningsveien 1, 0373 Oslo, Norway

[⊥]Haldor Topsøe A/S, Haldor Topsøes Allé 1, 2800 Kongens Lyngby, Denmark

[#]European Synchrotron Radiation Facility, 71 avenue des Martyrs, CS 40220, 38043 Grenoble Cedex 9, France

Supporting Information

ABSTRACT: The direct conversion of methane to methanol (MTM) is a reaction that has the potential to disrupt a great part of the synthesis gas derived chemical industry. However, despite many decades of research, active enough catalysts and suitable processes for industrial application are still not available. Recently, several copper-exchanged zeolites have shown considerable activity and selectivity in the direct MTM reaction. Understanding the nature of the active site in these materials is essential for any further development in the field. Herein, we apply multivariate curve resolution analysis of X-ray absorption spectroscopy data to accurately quantify the fraction of active Cu in Cu-MOR (MOR = mordenite), allowing an unambiguous determination of the active site nuclearity as a dicopper site. By rationalizing the compositional parameters and reaction conditions, we achieve the highest methanol yield per Cu yet reported for MTM over Cu-zeolites, of 0.47 mol/mol.



1. INTRODUCTION

The global stock of methane from shale gas, hydrates, and coalbed methane is constantly increasing,¹ but the transportation and processing are challenging.² Routes that can transform methane to high-value chemicals directly, avoiding the highly energy-consuming syngas route, are therefore economically and environmentally desirable. Reactive coupling of methane enables the direct production of olefins and aromatics in a high-temperature operation.³ Direct oxidation of methane requires milder conditions but suffers from both low conversion and selectivity or involves costly oxidants.^{2,4,5} Inspired by methanotrophic enzymes with copper in active complexes,⁶ researchers were able to mimic the sites that are found in nature in the confined environment of zeolite pores.^{7,8} The resulting materials are able to cleave the C–H bond and stabilize a methyl group that is later hydrolyzed into methanol.⁹ Until now, different zeolite frameworks (i.e., MFI,^{7,10} mordenite (MOR),^{9,11–14} and chabazite (CHA)^{15,16}) have been demonstrated to stabilize Cu in active sites (AS). The direct conversion of methane to methanol (MTM) over these materials involves three consecutive steps:

high-temperature activation in O₂, CH₄ loading at 200 °C, and finally extraction of the products with steam.

The MOR structure has straight 12-membered ring pores (12MR; 7.0 × 6.5 Å), interconnected by 8MR channels (5.7 × 2.6 Å) that are very narrow in one place, leading to what can more precisely be described as the 8MR side pockets. Cu is preferentially exchanged into these side pockets, where it balances the framework charge, forming active Cu_xO_y species upon activation in O₂.^{12,13,17,18} The exact nature and diversity of Cu centers formed during high-temperature oxidative treatment is still under debate. Currently, dinuclear^{9,19–23} or trinuclear¹³ Cu-oxo species have been proposed as the most favorable AS for methane activation. Recently, the effect of the aluminum content in the MOR framework was addressed leading to the conclusion that both monomeric as well as dimeric Cu species can be present and active for the conversion.²⁴ It appears that the speciation of Cu in MOR goes beyond the single-site paradigm and that it can be

Received: July 30, 2018

Published: October 22, 2018

66 dynamically transformed, influenced by composition as well as
67 by synthesis and pretreatment conditions, as demonstrated for
68 the CHA framework.^{16,25,26}

69 Herein, we evaluated Cu-MOR zeolites of different
70 composition for the MTM conversion. The normalized
71 product yields per Cu indicate a uniform population of active
72 sites, with the exception of one sample, where the maximum
73 stoichiometry of a dicopper AS—of almost 0.5 mol of
74 CH₃OH/mol Cu, is reached. Aiming to rationalize this unique
75 behavior, we exploited X-ray absorption spectroscopy (XAS)
76 to shed light on the nature of Cu ions in the MOR zeolite. The
77 subtle differences between active and inactive Cu^{II} species
78 formed during O₂ activation call for advanced experimental
79 and analytical approaches, to add species sensitivity to the
80 absorbing-atom-averaged XAS response. Additionally, the
81 duration of the key reaction steps is observed to largely
82 impact the product yield, requiring the use of consistent
83 reaction conditions for spectroscopy and testing. Having
84 fulfilled these requirements, we show how multivariate curve
85 resolution (MCR) analysis of in situ high-energy-resolution
86 fluorescence-detected (HERFD) X-ray absorption near edge
87 structure (XANES) can enable an accurate quantification of
88 the fraction of active Cu in O₂-activated Cu-MOR, allowing an
89 unbiased and unequivocal determination of the AS nuclearity
90 as a dicopper site.

2. METHODS

91 **2.1. Cu-MOR Synthesis and Physicochemical Character-**
92 **ization.** Commercial zeolites CBV21A (NH₄-MOR, Si/Al = 11) and
93 CBV10ADS (Na-MOR, Si/Al = 7) from Zeolyst Inc. were utilized as
94 parent materials. The first was once and the latter was three times ion
95 exchanged with NH₄NO₃ (10 wt % in water) at 60 °C for 5 h. Both
96 were washed NO₃-free; no Na was detected by energy-dispersive X-
97 ray spectroscopy (EDX). NH₃ was burned off by heating (1 °C/min)
98 in air at 500 °C for 8 h; afterward, the resulting H-form zeolites were
99 cooled to room temperature (RT), slowly rehydrated in air, and then
100 exchanged. Aqueous solutions (60 mL/g) of copper(II) acetate
101 (99.99%, Sigma-Aldrich) with 0.005 to 0.02 M were utilized for the
102 exchange, which was conducted under stirring at RT overnight. The
103 pH was adjusted during the exchange, with NH₄OH-solution (28%,
104 Sigma-Aldrich) and 0.1 M HNO₃, between 5.2 and 5.7. After
105 exchange, the materials were washed three times with water to remove
106 excess copper ions and avoid overloading. Standard physicochemical
107 analysis of all the investigated materials was performed by X-ray
108 diffraction (XRD), scanning electron microscopy—energy-dispersive
109 X-ray spectroscopy (SEM-EDX), N₂-physisorption, and ²⁷Al magic-
110 angle spinning (MAS) NMR spectroscopy as described in [Supporting](#)
111 [Information, Section S1](#).

112 **2.2. Testing for MTM Conversion over Cu-MOR.** Cu-MOR
113 zeolites were evaluated with respect to the activity toward MTM
114 conversion in a quartz plug flow reactor (ID = 6 mm). The
115 temperature was controlled by a tubular oven monitored by a
116 thermocouple placed in the center of the bed. For each measurement
117 100 mg of powder was utilized. Before the sample was pressed in
118 pellets, it was ground and sieved to obtain uniform particles in the
119 250–425 μm range. The stepwise MTM process included the
120 following three steps: (i) activation in oxygen at high temperature;
121 (ii) reaction with methane; (iii) extraction of methanol with steam.
122 Between each step the materials were flushed with He. In the
123 reference testing conditions, the Cu-MOR powder was initially dried
124 in He flow (15 mL/min) at 150 °C; afterward, an O₂ flow (15 mL/
125 min) was introduced, and the temperature increased with 5 °C/min
126 to 500 °C, where it stayed for 480 min. After activation, the
127 temperature was decreased to 200 °C with a rate of 5 °C/min in O₂.
128 The sample was then purged with He for 60 min before CH₄ loading
129 step; 15 mL/min CH₄ flow for 360 min at 200 °C. After the loading
130 step, the sample was purged again, and online H₂O-assisted extraction

of CH₃OH was performed isothermally. A flow of Ne/He (13.5 mL/
131 min) was passed through a saturator containing deionized water at 44
132 °C. After the purging step, the steam was introduced to the sample,
133 and the effluent was analyzed by a Hewlett-Packard 6890/5972
134 GCMS System. This protocol was repeated using shorter O₂
135 activation and CH₄ loading steps in the *operando* XAS testing
136 conditions and in the HERFD XANES testing conditions (see
137 [Supporting Information, Section S2](#) for a detailed overview).

138 **2.3. Operando XAS.** *Operando* XAS experiments were performed
139 at the BM31 beamline (Swiss Norwegian Beamline (SNBL)) of the
140 European Synchrotron Radiation Facility (ESRF; Grenoble, France).
141 We collected Cu K-edge XAS spectra in transmission mode, using a
142 water-cooled flat Si [111] double crystal monochromator. To measure
143 the incident (I₀) and transmitted (I₁) X-ray intensity, 30 cm length
144 ionization chambers filled with a mixture of He and Ar were used.
145 Continuous scans were performed in the 8800–10 000 eV range, with
146 a constant energy step of 0.5 eV. Collection of one XAS spectrum
147 required 10 min. We characterized the O₂-activated state for each
148 material collecting two consecutive scans and averaging the
149 corresponding μ(E) curves after checking for signal reproducibility.
150 For the measurements, the Cu-MOR powder was ground and sieved
151 with 250–212 μm sieves; ca. 3 mg of powder was then packed in a
152 capillary reactor (1 mm diameter) connected to an appropriate gas-
153 flow setup for the stepwise MTM reaction. Temperature at the
154 measurement position was controlled by a heat gun. A total flow rate
155 of 2 mL/min was employed for all the reaction steps, including O₂
156 activation at 500 °C in pure O₂ (90 min), pure CH₄ loading at 200 °C
157 (120 min), and CH₃OH extraction by steam admission at 200 °C (70
158 min). The heating and cooling ramps were always performed using a
159 rate of ±5 °C/min. For the extraction step, a flow of Ne/He was
160 passed through a saturator containing deionized water at 44 °C. The
161 steam was then introduced to the sample, and the effluent was
162 analyzed by a quadrupole mass spectrometer (MS; Pfeiffer Vacuum),
163 to quantify the productivity for investigated samples at the *operando*
164 XAS conditions. XAS spectra were normalized to unity edge jump
165 using the Athena software from the Demeter package.²⁷ The
166 extraction of the χ(k) extended X-ray absorption fine structure
167 (EXAFS) functions was also performed using Athena program, and R-
168 space EXAFS spectra were obtained by calculating the Fourier
169 transform of the k²χ(k) functions in the (2.4–8.7) Å⁻¹ k-range.
170

171 **2.4. In Situ HERFD XANES.** HERFD XANES measurements were
172 performed at the ID26 beamline of the ESRF. The spectra were
173 acquired in fluorescence mode, detecting only photons whose energy
174 corresponded to the maximum intensity of the Cu K_{β1,3} emission line
175 (~8906 eV). This energy selection was performed using five Si [553]
176 analyzer crystals (θ = 79.92°), set up in vertical Rowland geometry,
177 resulting in spectra resolution of 1.06 eV (elastic peak). The crystals
178 were spherically bent following the Johann scheme to focus the
179 fluorescence radiation onto an avalanche photodiode (APD) detector.
180 For the incident beam a flat double-crystal Si [311] monochromator
181 was employed. The time acquisition for each spectrum was set to 2
182 min.

The measurements were conducted using a well-established gas-
183 flow setup, based on the Microtomo reactor cell (developed by the
184 ESRF Sample Environment team),²⁸ that allowed to precisely control
185 the gas composition and the temperature inside, as described in
186 details in our previous works.^{29,30} The Cu-MOR samples were
187 prepared in the form of self-supporting wafers (ca. 100 mg of sample)
188 and fixed inside the reactor cell. In situ experiments during He and O₂
189 activation were performed heating the samples from 60 to 500 °C
190 with a heating ramp of 5 °C/min and flowing in the Microtomo
191 reactor cell 100 mL/min gas He or O₂, depending on the type of
192 pretreatment. The evolution of the XANES during the temperature
193 ramp was continuously monitored by 2 min scans. After the samples
194 were kept 30 min at 500 °C in He or in O₂, five additional scans were
195 collected and averaged to obtain a higher-quality HERFD XANES
196 spectrum. In addition, for the two Si/Al = 7 samples, a He-activated +
197 O₂ state was characterized. The samples were kept at 500 °C in He for
198 240 min and subsequently exposed to pure O₂ at the same
199 temperature; five HERFD XANES were collected after 120 or 150
200

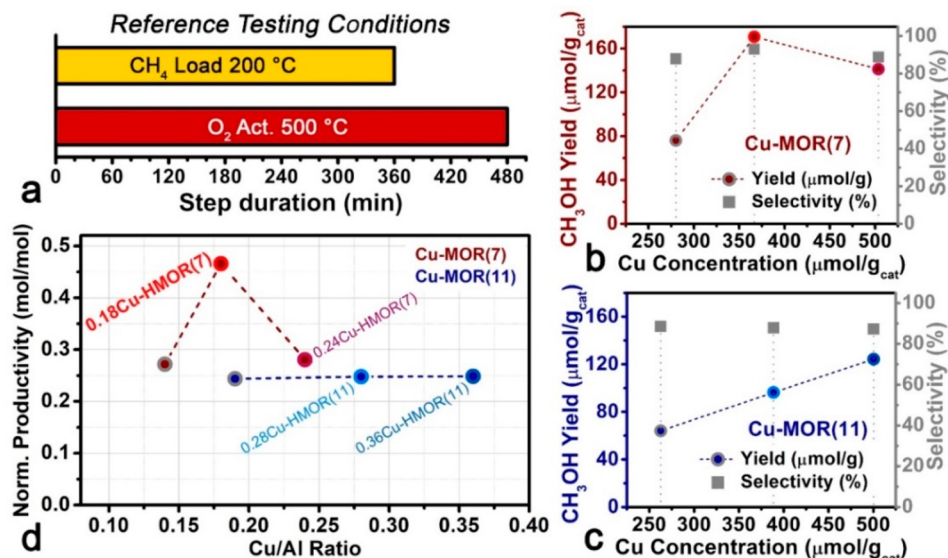


Figure 1. (a) Bar plot representing the duration of the O₂ activation and CH₄ loading steps at the reference testing conditions adopted to obtain the productivity values reported in the figure. For detailed reaction conditions, see [Methods](#) and [Supporting Information](#), Section S2. (b, c) CH₃OH yield (μmol CH₃OH/g_{cat}, colored circles, left ordinate axis) and selectivity (%), gray squares, right ordinate axis) as a function of Cu concentration (μmol Cu/g_{cat}) for Cu-MOR materials with Si/Al = 7 (b, Cu-MOR(7) series) and Si/Al = 11 (c, Cu-MOR(11) series). (d) Normalized productivity (mol CH₃OH/mol Cu) as a function of the Cu/Al ratio, comparing the Cu-MOR(7) and the Cu-MOR(11) series. The four samples selected for spectroscopic characterization are highlighted with colored contours, using the same color code as in the following figures.

201 min in O₂ at 500 °C, for 0.18Cu-HMOR(7) and 0.24Cu-HMOR(7),
 202 respectively, and then averaged as described before. All the collected
 203 HERFD XANES spectra were normalized to unity edge jump using
 204 the Athena software from the Demeter package.²⁷

205 **2.5. MCR-ALS Analysis.** Multivariate curve resolution (MCR) is
 206 an emerging data analysis technique, allowing to model an
 207 experimental data set **D** (including q spectra), as the product of an
 208 **S** matrix, composed by N (with $N < q$) pure spectra and a matrix **C**,
 209 which elements correspond to signal-related concentration profiles: \mathbf{D}
 210 $= \mathbf{C} \mathbf{S}^T + \mathbf{E}$, where \mathbf{S}^T is the transpose of matrix **S**, while **E** represents
 211 the error matrix associated with the reconstruction. To this aim, the
 212 Multivariate Curve Resolution Alternating Least Squares (MCR-ALS)
 213 algorithm employed in this work performs the dissociation optimizing
 214 concentration profiles and pure spectra in an altering least-squares
 215 under constraints.^{31–33} The first step of the algorithm requires the
 216 determination of the number of statistically significant components in
 217 the experimental data matrix. To this purpose, we performed principal
 218 component analysis (PCA).³⁴ As described in the Supporting
 219 Information, Section S8, PCA indicated five principal components
 220 in the data set reported in [Figure 3a](#). For MCR-ALS analysis we
 221 employed the graphical user interface (GUI) by Jaumot and co-
 222 workers,³⁵ freely downloadable at <http://www.mcrals.info/>, using
 223 Matlab R2011b. The analyzed data set globally consisted in a column-
 224 wise augmented matrix obtained by joining the four HERFD XANES
 225 data sets collected on 0.18Cu-HMOR(7) and 0.36Cu-HMOR(11)
 226 during O₂ activation and He activation (45 scans for each subdata set,
 227 180 scans in total). For MCR, the spectra were analyzed in the 8975–
 228 9021 eV energy range, including 460 energy points. The initial
 229 unmixing data procedure was performed using the SIMPLISMA
 230 algorithm,³⁶ with an allowed noise parameter fixed at 5%.³¹ The ALS
 231 routine was run employing the following *soft* constraints: non-
 232 negativity for both pure spectra and concentration profiles (using the
 233 fast non-negative least-squares algorithm, *fnnl*³⁷) and closure to 1 for
 234 the concentration profiles (permitted since an element-selective
 235 technique is employed, probing all the Cu in the system). The
 236 optimization routine successfully converged after 20 iterations,
 237 resulting in the final ALS quality control parameters shown in the
 238 [Supporting Information](#), Table S7.

3. RESULTS

239 **3.1. Composition-Productivity Trends for MTM over**
Cu-MOR. Cu-exchanged mordenites (Cu-MOR) were synthe-
 240 sized via liquid ion exchange of the parent H-form (HMOR, Si/Al = 11
 241 and Si/Al = 7) and denoted as x Cu-HMOR(y) where x and y represent the Cu/Al and Si/Al ratios,
 242 respectively. Microscopy reveals partially agglomerated crystals
 243 in the range from 50 to 300 nm, without detectable Cu
 244 nanoparticles. Additional details on the synthesis as well as the
 245 physicochemical characterization of the parent and Cu-
 246 exchanged mordenite zeolites can be found in the [Methods](#)
 247 as well as in the [Supporting Information](#).²⁴⁹

250 The synthesized Cu-MOR zeolites were evaluated for their
 251 activity in the MTM reaction. The samples were first activated
 252 at 500 °C in O₂ flow for 480 min then reacted with CH₄ at 200
 253 °C for 360 min ([Figure 1a](#)); finally, the products were
 254 extracted with steam isothermally and analyzed by an online
 255 MS; see also [Methods](#) and [Supporting Information](#), Section S2.
 256 The methanol output is illustrated in [Figure 1b,c](#) as yield per
 257 gram of sample (μmol/g) as well as normalized by Cu content
 258 (mol/mol, [Figure 1d](#)). The Cu-MOR samples with Si/Al = 11
 259 exhibit a linear trend of the yield with increasing Cu loading,
 260 reflected in an almost constant normalized productivity (ca.
 261 0.25 mol/mol). A similar behavior is exhibited by the materials
 262 with Si/Al = 7 having the lowest and the highest Cu-loading in
 263 the series. These findings are in line with previous reports for
 264 Cu-MOR. Here, the density of active sites is mostly found
 265 proportional to the Cu concentration, translating into a similar
 266 normalized productivity/selectivity for materials with the same
 267 Si/Al ratio and indicating a uniform nature of the AS
 268 throughout the compositional space.^{12,13}

269 However, the material with intermediate Cu loading (Cu/Al
 270 = 0.18) exhibits an outstanding performance, yielding 170
 271 μmol/g_{cat}. The nuclearity of the AS reported for similar Cu-
 272 MOR materials has been proposed to vary from two to three
 273 Cu atoms. From the data reported in [Figure 1](#), it appears that

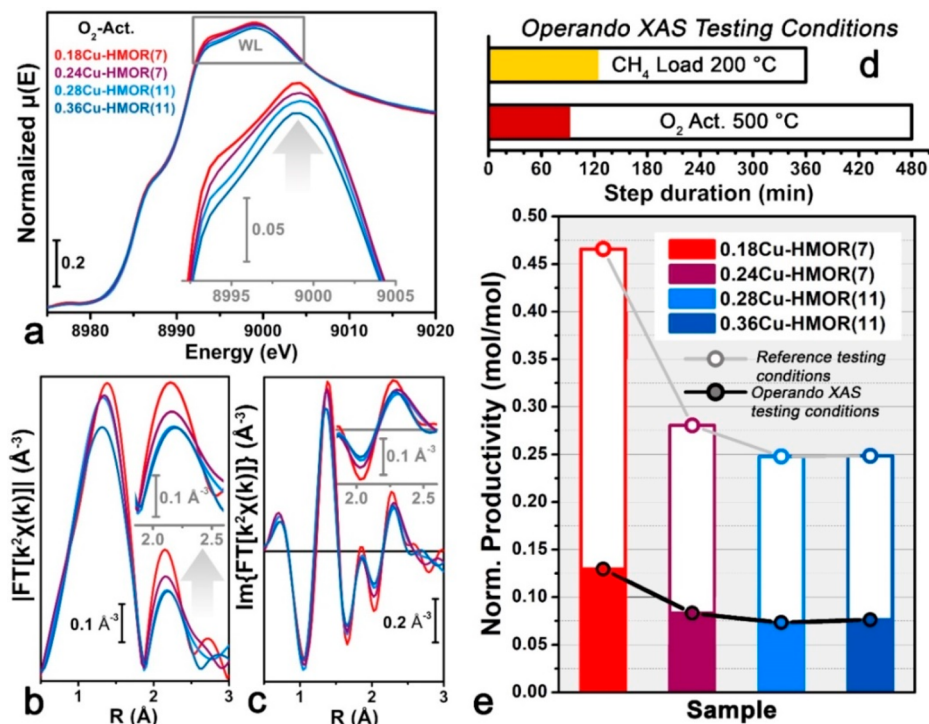


Figure 2. (a) Normalized Cu K-edge XANES spectra of selected Cu-MOR samples after O₂ activation at 500 °C. (inset) A magnification of the so-called WL peak, highlighted by the gray box in the main panel. Magnitude (b) and imaginary part (c) of the corresponding phase-uncorrected FT-EXAFS spectra. (insets b, c) A magnification of the second-shell peak. (d) Bar plot comparing the duration of the O₂-activation and CH₄ loading steps under the *operando* XAS conditions (colored portion of the bars) and the reference conditions. (e) Corresponding normalized productivity at the *operando* XAS conditions (full colored bars and circles) in comparison with the reference testing conditions (empty bars and circles). In all the panels, the same color code is used to identify the different investigated materials.

274 the 0.18Cu-HMOR(7) sample, with a normalized productivity
275 of ca. 0.47 mol/mol, performs close to the maximum value
276 allowed by the stoichiometry assuming a dicopper AS,
277 exhibiting a uniquely high density of active species.

278 It should be emphasized that the performance of this
279 material was fully reproducible, also when starting with the
280 introduction of Cu into the same zeolite (see Figure S4 in the
281 Supporting Information). To assess the impact of the zeolite
282 synthesis on the outstanding performance of 0.18Cu-
283 HMOR(7), we synthesized *ex novo* a Cu-MOR zeolite in
284 house, targeting the same composition (Si/Al = 7 and Cu/Al =
285 0.18). Our efforts resulted in the 0.20Cu-HMOR(7)_{en}
286 sample with Si/Al = 7 and Cu/Al = 0.20. As reported in the
287 Supporting Information (Section S4), the newly prepared
288 material at the reference MTM testing conditions gives a
289 normalized CH₃OH yield of 0.19 mol/mol, not comparable
290 with the performance of 0.18Cu-HMOR(7). Taken together,
291 these results indicate an optimum combination of zeolite
292 synthesis parameters, Si/Al ratio (both key factors in
293 determining the framework Al distribution), and Cu-loading
294 with respect to methanol yield. Nonetheless, to determine the
295 exact fraction of active Cu over total Cu, the AS nuclearity
296 needs to be independently proven, while linking the singular
297 performance of 0.18Cu-HMOR(7) to an atomic-scale under-
298 standing of Cu-speciation across the compositional series.

299 **3.2. Cu Active Site Spectroscopic Fingerprints from**
300 **Operando XAS.** To rationalize the composition-productivity
301 trends highlighted above, we initially applied *operando* XAS at
302 the Cu K-edge. We selected two representative materials for
303 each Si/Al ratio, namely, 0.18Cu-, 0.24Cu-HMOR(7) and
304 0.28Cu-, 0.36Cu-HMOR(11). Using a capillary reactor, we

performed the MTM reaction cycle over each material, while
305 monitoring the average electronic and structural properties of the
306 Cu ions by XAS (see also Methods).

307 The methane-converting Cu sites are formed during the
308 high-temperature activation step in an oxidizing atmos-
309 phere.^{16,38} Hence, we focus on the comparison of the
310 XANES and EXAFS spectra of the O₂-activated materials,
311 reported in Figure 2a and Figure 2b,c, respectively.

312 The XANES features can be interpreted based on previous
313 studies on Cu-MOR^{13,20} and other Cu-zeolites.^{16,25,29,30,39} For
314 all the samples, O₂ activation results in a virtually pure Cu^{II}
315 state; no Cu^I contribution is observed within the detection
316 limit. The XANES spectra of the four Cu-MOR zeolites show
317 remarkable similarities, thus revealing comparable coordination
318 environments for the Cu ions in the pores. Nonetheless, a
319 trend is observed in the intensity of the so-called white-line
320 (WL) peak at ca. 9000 eV in the XANES (faded gray arrow in
321 the inset of Figure 2a). Low Si/Al and low Cu/Al both appear
322 to promote a higher WL intensity, with the outperforming
323 0.18Cu-HMOR(7) showing the highest WL peak.

324 A higher WL intensity in Cu K-edge XANES is commonly
325 associated with a higher coordination number in the first shell
326 of the cation, as well as to a more uniform bond length
327 distribution. The Fourier transform (FT) EXAFS spectra in
328 Figure 2b,c confirm this observation. The intensity of the first-
329 shell peak, stemming from scattering contributions by
330 framework (O_{fw}) and extra-framework (O_{ef}) oxygen atoms,
331 follows the same trend. The EXAFS for the four materials also
332 shows a well-defined peak in the second-shell region, extending
333 from 2 to 3 Å in the phase-uncorrected spectra. Guided by
334 previous studies,^{16,20,25,30,39} we expect both Al and Si atoms
335

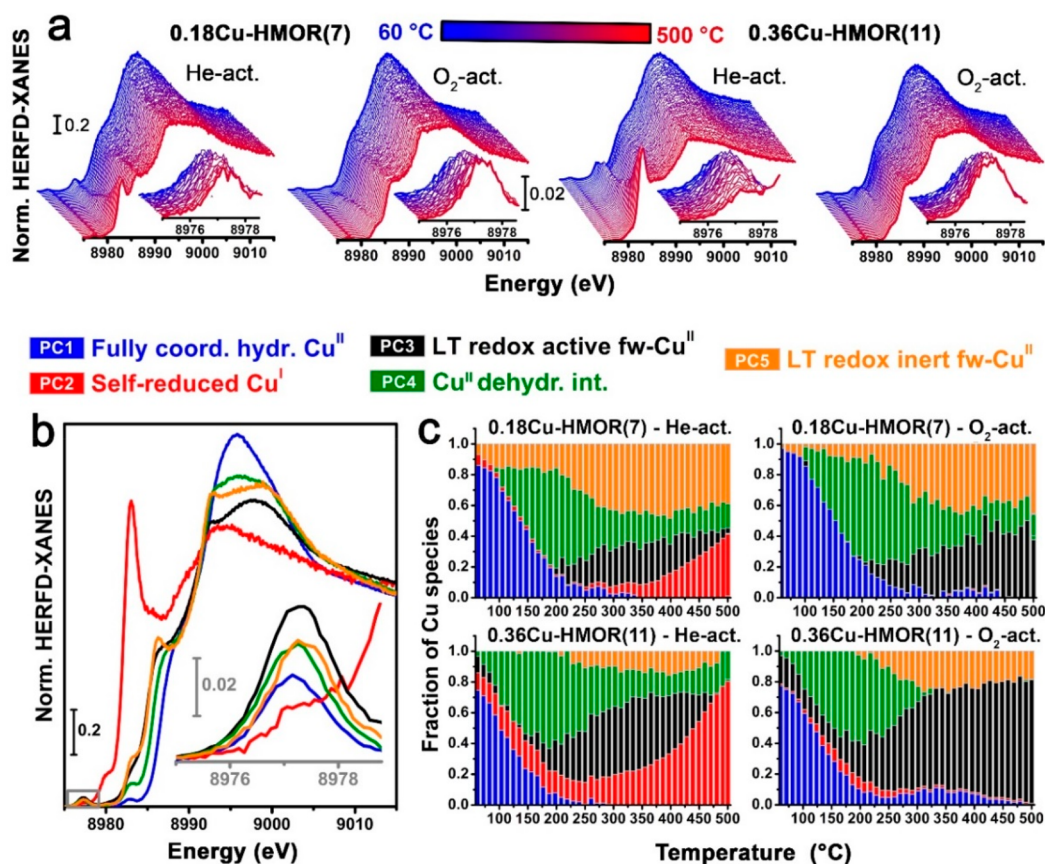


Figure 3. (a) Time-dependent HERFD XANES collected on 0.18Cu-HMOR(7), left panels, and 0.36Cu-HMOR(11), right panels, during thermal treatment in O₂ and He gas flow from 60 °C (blue curves) to 500 °C (red curves), using a heating rate of 5 °C/min (ca. 90 min for each experiment). (insets) A magnification of the weak pre-edge peak mostly deriving from the dipole-forbidden 1s → 3d transition in d⁹ Cu^{II} centers. (b) Theoretical “pure” HERFD XANES spectra of Cu-species from MCR analysis of the data set in (a). (c) Corresponding temperature-dependent concentration profiles of each Cu species. In a similar way as recently found for Cu-CHA,⁴³ pseudo-octahedral Cu^{II} aquo complexes (PC1) undergoes partial dehydration to four-coordinated Cu^{II} species (PC4). These Cu^{II} dehydration intermediates reach maximum concentration at ~200 °C and then progressively convert into framework-interacting Cu^{II} species (fw-Cu^{II}). Among these, a low-temperature (LT) redox-active component (PC3) is found, efficiently undergoing reduction to Cu^I (PC2) in inert atmosphere from 250 °C upward. An LT redox-inert component is also identified (PC5): it remains stable in He up to 400 °C and is more abundantly formed in the highly active 0.18Cu-HMOR(7) material.

336 belonging to the framework (T_{fw}) and Cu–Cu scattering from
 337 Cu_xO_y multimetric moieties to contribute in this R-space range.
 338 Notably, this peak undergoes intensity modifications as a
 339 function of the composition (insets of Figure 2b, faded gray
 340 arrow). 0.18Cu-HMOR(7) displays the highest intensity,
 341 followed by 0.24Cu-HMOR(7) and then by the two Si/Al =
 342 11 samples. The latter show an equivalent development of the
 343 EXAFS features in this R-space range.

344 After 90 min in O₂ at 500 °C, the samples were cooled to
 345 200 °C and reacted with methane for 120 min. MS analysis of
 346 the reactor effluent during the steam-assisted CH₃OH
 347 extraction (see also Supporting Information, Section 5.2)
 348 allowed for online quantification of the yield. Figure 2e
 349 compares the normalized productivity evaluated under the
 350 *operando* XAS conditions (Figure 2d) as well as under the
 351 reference testing conditions (Figure 1a). The results
 352 demonstrate that our materials were active under the XAS
 353 conditions, although the normalized productivity is on average
 354 (71 ± 1)% lower compared to the reference conditions. This
 355 decrease points out how the duration of the key reaction steps
 356 affect the methanol yield,¹⁶ while exactly the same activity
 357 trend is maintained.

Intriguingly, the normalized productivity directly correlates 358
 with the intensity of the second-shell peak in the EXAFS 359
 spectra. A higher second-shell peak associates with a higher 360
 fraction of active Cu in the materials. Cu– T_{fw} scattering 361
 contributions are expected to be equally present into both 362
 monomeric and multimetric Cu^{II} moieties coordinated to O_{fw} 363
 atoms at well-defined exchange sites in the zeolite framework 364
 (fw-Cu^{II}), and we attribute the increased intensity to a stronger 365
 Cu–Cu contribution. EXAFS thus provides direct structural 366
 evidence for multicopper active sites in Cu-MOR. Nonetheless, 367
 the relatively low abundance of active species formed at the 368
 XAS conditions, together with the limited contrast between the 369
 spectral signatures of active and inactive Cu^{II}, hampers the 370
 quantification of the fraction of active Cu from the *operando* 371
 XAS data in Figure 2. 372

3.3. Enhancing the Spectroscopic Contrast by MCR 373
Analysis of HERFD XANES. Aiming at a quantitative 374
 understanding of the structure–activity relationships for Cu- 375
 MOR, we measured sequences of HERFD XANES spectra 376
 during high-temperature treatment in O₂ and He gas flow for 377
 0.18Cu-HMOR(7) and 0.36Cu-HMOR(11) (see Methods for 378
 experimental details). Indeed, monitoring the resistance of 379
 different fw-Cu^{II} species to the so-called self-reduction (well- 380

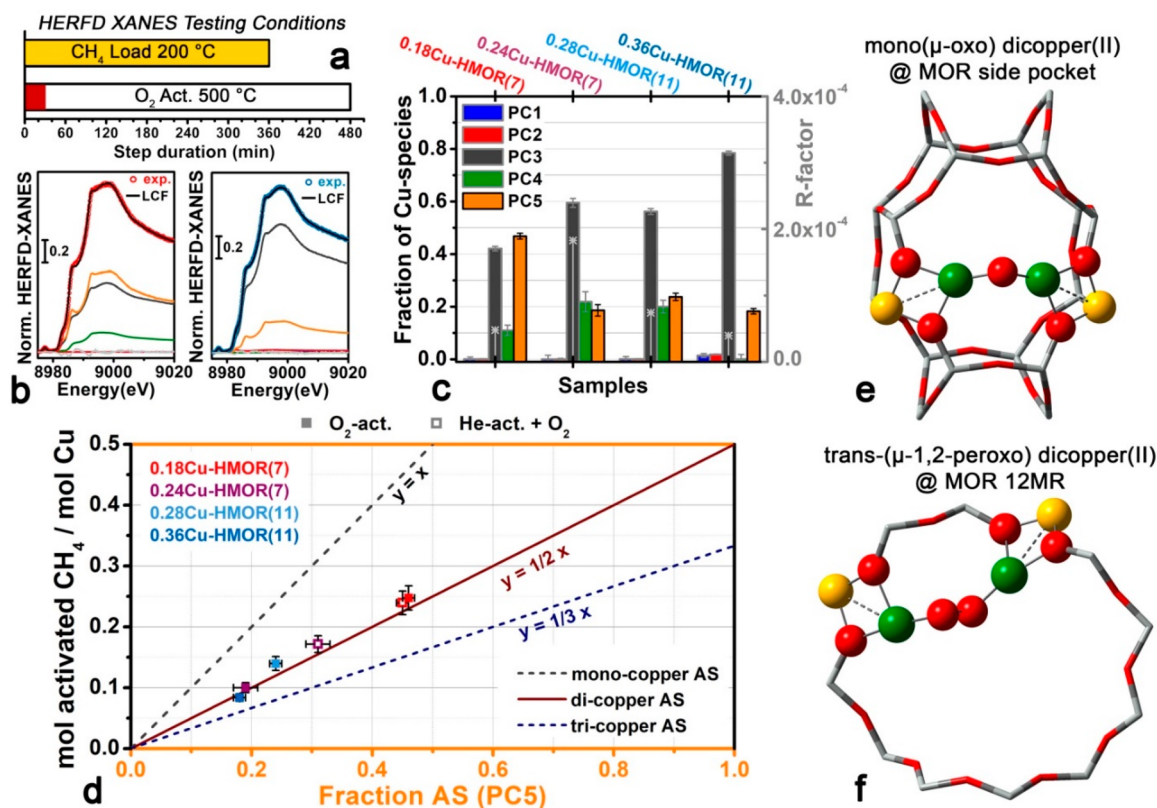


Figure 4. (a) Bar plot representing the duration of the O₂ activation and CH₄ loading steps at the HERFD XANES testing conditions, adopted into parallel laboratory tests to effectively correlate spectroscopy results and performance. (b) Comparison between experimental HERFD XANES of representative O₂-activated Cu-MOR samples, namely, 0.18Cu-HMOR(7) and 0.36Cu-HMOR(11), with the corresponding best-fit curves from LCF analysis, using the pure spectra from MCR analysis (Figure 3b) as references. For each fitted spectrum, the LCF components scaled by their respective optimized weights, and the LCF residuals are reported (the same information for the whole set of samples can be found in the Supporting Information, Section S9). (c) Cu speciation in the O₂-activated Cu-MOR series as determined from LCF analysis of HERFD XANES spectra. The Cu species (PC1-PC5) are denoted using the same color code as used in Figure 3b,c. The LCF R-factor is also reported (gray stars, right ordinate axis). (d) Quantitative correlation between the normalized productivity evaluated at the HERFD XANES testing conditions and the fraction of LT redox-inert fw-Cu^{II} (PC5—our presumed AS) from LCF analysis (O₂ activation: full colored symbols; He activation + O₂: empty colored symbols). All the experimentally determined values match the ideal trend line for stoichiometric conversion over a dicopper AS, reported as a full dark red line. (e, f) Illustrations of possible Cu₂O_x AS in the MOR framework compatible with the experimental results reported here, namely, (e) a mono(μ-oxo) dicopper(II) core in the MOR side pocket and (f) a trans-(μ-1,2-peroxo) dicopper(II) core in the MOR 12MR. Atom color code: Cu, green; O, red; Si, gray; Al, yellow.

381 known to occur in Cu zeolites during thermal treatment in
 382 inert conditions^{20,30,40–42}) can assist their identification.^{25,43} In
 383 parallel, the higher energy resolution, ensured by using an X-
 384 ray spectrometer,^{44,45} was crucial to successfully resolve the
 385 XANES of active and inactive Cu.

386 Figure 3 displays the evolution of the HERFD XANES for
 387 the two Cu-MOR samples as a function of the temperature,
 388 from 60 to 500 °C. The XANES evolution up to ca. 250 °C is
 389 only weakly affected by the gaseous environment. All the
 390 observed spectral modifications in this temperature window are
 391 consistent with thermally driven dehydration of the Cu
 392 centers.^{20,30,43} However, at higher temperatures, the pretreat-
 393 ment environment drastically impacts the XANES features,
 394 resulting in distinct O₂- and He-activated final states. The
 395 HERFD XANES spectra at 500 °C in O₂ match the
 396 corresponding conventional XANES in Figure 2a, indicating
 397 a dominant contribution from fw-Cu^{II} species. Considerably
 398 more defined peaks are observed, in line with the better
 399 detection scheme. In contrast, a substantial population of Cu^I
 400 species is detected at 500 °C in He. The intense peak
 401 developing at 8983 eV points to quasi-linear Cu^I config-

urations,⁴⁶ in line with earlier observations for Cu-MOR¹⁹ and
 Cu-MFI.⁴⁷

Similar XANES features are well-documented to develop
 during interaction of O₂-activated Cu zeolites with CH₄,
 resulting in the formation of Cu^I ions.^{9,13,16,21,48} In this respect,
 Netwon et al.⁴⁸ have recently evaluated by Cu K-edge XANES
 the fraction of Cu^I formed during the CH₄-loading step of the
 MTM process over various Cu zeolites. The results are
 correlated to the methanol yield, as determined by
 independent reactor-based tests. Therein, the authors highlight
 a general relationship between the fraction of Cu^I and the
 methanol productivity, consistent with a two-electron CH₄
 conversion mechanism based on Cu^{II}/Cu^I redox couples.
 Hereafter, we will look the problem from a different angle, that
 is, determining and correlating with the productivity per Cu
 the fraction of active Cu species formed during O₂ activation,
 to quantitatively assess the AS nuclearity.

Notably, the outperforming 0.18Cu-HMOR(7) appears to
 be more resistant to self-reduction compared to 0.36Cu-
 HMOR(11). Indeed, it shows an almost halved intensity of the
 Cu^I peak at 8983 eV, a significantly higher Cu^{II} 1s → 3d pre-

edge peak, and a WL peak more similar to what is otherwise observed after O₂ activation. We employed statistical analysis and MCR on the large HERFD XANES data set in Figure 3a to resolve the spectra and concentration profiles of the Cu-species formed in the two Cu-MOR samples as a function of temperature and activation conditions. Principal component analysis (PCA, see Supporting Information, Section 8.1) indicated that the whole data set can be described by linear combinations of the spectra of five Cu species. The actual spectra of the five Cu species were obtained by an MCR algorithm, as detailed in the Methods. The MCR results are summarized in Figure 3b,c reporting the theoretical HERFD XANES spectra and their concentration profiles for the tested material/activation protocols combinations.

The characteristic XANES features of the theoretical spectra, together with their temperature-dependent dynamics, provide the basis for their assignment, as detailed in the caption of Figure 3. MCR analysis reveals two fw-Cu^{II} species, characterized by different resistance toward self-reduction, and distinct XANES features. One type of fw-Cu^{II} is found to efficiently reduce to Cu^I already at 250 °C in He (low-temperature (LT) redox-active fw-Cu^{II}, PC3 in Figure 3b,c). In contrast, the species referred to as LT redox-inert fw-Cu^{II} (PC5 in Figure 3b,c), remains stable until 400 °C in inert atmosphere. This behavior is consistent with the higher stability predicted for multimetric Cu-oxo cores,⁴⁹ with respect to monomeric Cu^{II} species. The latter could include [Cu^{II}OH]⁺, [Cu^{II}O]⁺, and, in the presence of O₂, [Cu^{II}O₂]⁺ formed at a single-Al docking site during dehydration.

LT redox-inert fw-Cu^{II} is significantly more abundant in the highly productive 0.18Cu-HMOR(7). Its XANES is characterized by more intense and sharper peaks with respect to the LT redox-active component, especially in the WL region. LT redox-inert fw-Cu^{II} (PC5) is observed in both inert and oxidizing environments, which supports anaerobic pathways as a viable alternative to direct routes involving molecular oxygen activation at Cu sites. With this respect, the formation of dicopper(II) cores from the condensation of neighboring [CuOH]⁺ species ($2 [\text{Cu}^{\text{II}}\text{OH}]^+ \rightarrow [\text{Cu}^{\text{II}}\text{OCu}^{\text{II}}]^{2+} + \text{H}_2\text{O}$),^{20,40,50} could represent a plausible hypothesis. Nonetheless, during a prolonged activation at 500 °C, an oxidizing environment appears necessary for its stabilization, in agreement with O₂ temperature-programmed desorption results for Cu-ZSM-5.⁵¹ Replicating the inert pretreatment conditions for the MTM reaction cycle over selected Cu-MOR samples resulted in a drastic productivity loss (see Supporting Information, Section S6). Under these conditions, the normalized productivity drops to 0.021 and 0.007 mol CH₃OH/mol Cu for 0.18Cu-HMOR(7) and 0.36Cu-HMOR(11), respectively, still pointing toward a higher residual activity for 0.18Cu-HMOR(7). All these lines of evidence are consistent with the *operando* XAS results and indicate the LT redox-inert fw-Cu^{II} (PC5 in Figure 3) as the active site for the MTM conversion over Cu-MOR. We note that what is here referred to as “the active site” most likely consists into a molecular-level distribution of Cu species (e.g., in correspondence of different Al positions in the framework²³) giving similar MTM activity and lumping into the same principle component in MCR-XANES analysis.

3.4. Quantitative Evidence for a Dicopper Active Site. We further characterized the same Cu-MOR materials investigated by *operando* XAS by collecting higher-quality HERFD XANES after the samples were kept at 500 °C in O₂

for 30 min. Using the pure spectra in Figure 3b as references, we applied linear combination fit (LCF) analysis to these higher-quality spectra, to accurately determine Cu-speciation in the complete set of samples (Figure 4b,c, see also Supporting Information, Section S9). Under these conditions, the outperforming 0.18Cu-HMOR(7) contains the highest fraction of LT redox-inert fw-Cu^{II} (PC5, 47% of total Cu). This is in contrast to the three other materials, where the LT redox-active species is promoted: it accounts for 52–78% of total Cu, at the expense of our presumed active site (PC5, 18–24%). Minor contributions from the Cu^{II} dehydration intermediate species (PC4) are also detected in all the samples except for 0.36Cu-HMOR(11).

The duration of each reaction step clearly has a strong impact on the performance of the tested materials (Figure 2e). Thus, we re-evaluated the four Cu-MOR zeolites under an ad hoc set of conditions (HERFD XANES testing conditions, Figure 4a). Here, the O₂-activation step is set to 30 min, as used in HERFD XANES experiments, whereas a 360 min-long CH₄ loading step is employed to efficiently saturate all the available active sites (see Supporting Information, Section S7). This ensures that the measured yield of C-containing products (CH₃OH and minor fractions of overoxidation products) per Cu is a trustworthy measure of the fraction of active Cu formed during the O₂-activation step at these conditions. Figure 4d correlates the thus-determined mol-activated CH₄/mol Cu with the fraction of LT redox-inert fw-Cu^{II} (PC5) from LCF analysis. The experimental points for our Cu-MOR sample series after O₂ activation (full colored circles in Figure 4d) accurately approximate the ideal trend line for stoichiometric MTM conversion over a dicopper AS (dark red line in Figure 4d), unambiguously demonstrating that two Cu ions are cooperatively involved in the activation of a CH₄ molecule over these materials. The same plot as in Figure 4d but reporting the mol CH₃OH/mol Cu versus fraction of PC5 can be found in Supporting Information (Section S10) together with some discussion about the process selectivity as a function of the AS abundance.

For the Si/Al = 7 Cu-MOR samples, we also investigated a different pretreatment, exposing He-activated materials to O₂ at 500 °C (see Supporting Information, Table S5). The corresponding experimental points, obtained correlating results of HERFD XANES LCF analysis and productivity per Cu evaluated after the same pretreatment, are reported as empty squares in Figure 4d. Thus, both for different materials and even when using different activation protocols for the same material, the points keep following the dicopper AS trend line, evidencing how the same dimeric active site is consistently conserved. Remarkably, a dicopper(II) AS is consistent with the results by Newton et al.,⁴⁸ supporting a mechanism based on the Cu^I/Cu^{II} redox couple rather than on the Cu^{II}/Cu^{III} one, or alternative routes involving Cu^{II}-O• radicals.

The pure HERFD XANES signature of PC5 and the structural insights from *operando* EXAFS both indicate that the Cu₂O_x AS is built up by threefold O-ligated Cu^{II} units, in a coordination motif fully consistent with the available models of the mono(μ -oxo) dicopper(II) core in Cu-zeolites^{10,19,23,47} (Figure 4e). Nonetheless, on the basis of our XAS results, a *trans*-(μ -1,2-peroxo) dicopper(II) core (Figure 4f), as recently proposed in Cu-CHA,⁵² cannot be ruled out. Having established the AS as a dicopper(II) species discourages the direct involvement of mononuclear [Cu(OH)]⁺ complexes stabilized in the proximity of an isolated 1-Al site, although 548

549 these species would possess a tridentate geometry analogue to
550 the one of the Cu_2O_x moieties depicted in Figure 4e,f. As
551 previously proposed for Cu-CHA,¹⁶ $[\text{Cu}(\text{OH})]^{+}$ species most
552 likely serve as precursors to form the active Cu_2O_x species,
553 through processes favored by activation at high temperature.
554 Reasonably, on the basis of our previous XANES-MCR results
555 about Cu-speciation in Cu-CHA,⁴³ it is plausible to connect
556 $[\text{Cu}(\text{OH})]^{+}$ with the PC3 component (LT redox-active fw-
557 Cu^{II}) found here for Cu-MOR. Overall, the fundamental
558 knowledge accessed here will pave the way to future research
559 aiming to assess in detail the identity of the dicopper AS in Cu-
560 MOR.

561 Projecting the normalized yield obtained at the reference
562 testing conditions (480 min-long O_2 activation) for 0.18Cu-
563 HMOR(7) on the spectroscopically validated dicopper AS
564 trend line, we estimate more than 90% of total Cu to be
565 coordinated in Cu_2O_x active species, resulting in the highest
566 productivity per Cu reported for MTM over Cu-exchanged
567 zeolites. Hence, prolonged exposure to O_2 at 500 °C promotes
568 important reorganization phenomena in the Cu ions siting,
569 resulting in the dynamic transformation of inactive Cu into
570 active species (or possibly precursor to active species). In the
571 presence of the most favorable compositional landscape, such
572 as in 0.18Cu-HMOR(7), these processes finally yield a *quasi-*
573 *single-site* catalyst, where virtually all Cu is organized into active
574 Cu_2O_x cores.

4. CONCLUSIONS

575 This study provides a novel perspective on the complex nature
576 and dynamics of Cu ions in the MOR framework and explores
577 the impact of these factors on the MTM conversion.
578 Compositional characteristics (Cu/Al and Si/Al ratios) appear
579 to determine an upper threshold for the productivity of the
580 materials. An optimum combination of framework Al
581 distribution (influenced by synthesis parameters and Si/Al
582 ratio) with Cu loading is shown to exist, enabling uniquely
583 high activity for methane activation, as seen for 0.18Cu-
584 HMOR(7). However, productivity in Cu-MOR can be further
585 modulated by adjusting the process conditions. Synergizing the
586 most favorable synthesis and compositional parameters and
587 reaction conditions, we obtained the highest methanol yield
588 per Cu yet reported for MTM over Cu-zeolites, of 0.47 mol/
589 mol.

590 Conventional XAS under *operando* conditions evidenced
591 specific fingerprints of the AS, revealing that both active and
592 inactive fw- Cu^{II} species coexist after O_2 activation. Enhancing
593 the spectroscopic contrast by MCR analysis of HERFD
594 XANES data, we captured the XANES signature of each Cu
595 species present in the MOR framework. This approach enabled
596 an accurate quantification of Cu speciation in the activated
597 materials. O_2 activation and CH_4 loading time were observed
598 to drastically impact the yield. Thus, we adopted consistent
599 protocols for both spectroscopy and testing to quantitatively
600 correlate Cu speciation to productivity per Cu. Furthermore,
601 we linked a specific fw- Cu^{II} moiety with the MTM AS (or
602 “pool” of ASs), characterized by a higher resistance toward self-
603 reduction and mostly favored in 0.18Cu-HMOR(7). We
604 directly correlated the abundance of such Cu^{II} species to the
605 yield of CH_4 oxidation products per Cu, over several
606 combinations of compositional and pretreatment parameters.
607 For the first time, the fraction of active Cu in Cu-MOR has
608 been quantified by a spectroscopic method and correlated with

performance at relevant conditions, to provide quantitative
evidence of the active site nuclearity.

Taken together, our results demonstrate that the active site
for selective methane oxidation over Cu mordenite is a
dicopper site. This is based on two strong observations. First,
we have prepared a material that activates nearly one methane
molecule per two Cu. Second, we show that across a series of
materials and activation protocols, the productivity increases
with a slope of exactly 0.5 when the spectroscopically
determined concentration of *active* Cu is increased. The
dynamics directing the speciation of Cu along activation, in
combination with the highly active material described, suggest
a clear direction for future research in the field.

■ ASSOCIATED CONTENT

Supporting Information

The Supporting Information is available free of charge on the
ACS Publications website at DOI: 10.1021/jacs.8b08071.

Physico-chemical characterization, additional experimen-
tal protocols and activity measurements, details on
operando XAS measurements, additional information on
MCR-ALS and LCF analyses (PDF)

■ AUTHOR INFORMATION

Corresponding Authors

*stian.svelle@kjemi.uio.no. (S.S.)

*pabb@topsoe.com. (P.B.)

*elisa.borfecchia@unito.it. (E.B.)

ORCID

Dimitrios K. Pappas: 0000-0002-6556-307X

Michael Dyballa: 0000-0002-8883-1145

Kirill A. Lomachenko: 0000-0003-0238-1719

Pieter Glatzel: 0000-0001-6532-8144

Bjørnar Arstad: 0000-0003-0398-786X

Carlo Lamberti: 0000-0001-8004-2312

Silvia Bordiga: 0000-0003-2371-4156

Unni Olsbye: 0000-0003-3693-2857

Stian Svelle: 0000-0002-7468-5546

Elisa Borfecchia: 0000-0001-8374-8329

Present Addresses

○Universitat Stuttgart, Pfaffenwaldring 55, 70174 Stuttgart,
Germany.

◆Center for Materials Science and Nanotechnology (SMN),
Department of Chemistry, University of Oslo, 1033 Blindern,
0315 Oslo, Norway.

Notes

The authors declare no competing financial interest.

■ ACKNOWLEDGMENTS

This publication forms a part of the iCSI (industrial Catalysis
Science and Innovation) Centre for Research-based Innova-
tion, which receives financial support from the Research
Council of Norway under Contract No. 237922. E.B. also
acknowledges Innovation Fund Denmark (Industrial postdoc
No. 5190-00018B). C.L. and A.M. acknowledge the Mega-
grant of the Russian Federation Government to support
scientific research at the Southern Federal University, No.
14.Y26.31.0001. We are grateful to W. van Beek for the
competent support during our XAS experiments at the BM31
beamline of ESRF. D. S. Wragg, M. Signorile, E. S. Gutterød, 665

666 and A. Lazzarini are acknowledged for support in the materials'
667 characterization and testing. K. P. Lillerud is acknowledged for
668 insightful discussions and advice on the chemistry of the
669 studied materials.

670 ■ REFERENCES

- 671 (1) Schwach, P.; Pan, X. L.; Bao, X. H. *Chem. Rev.* **2017**, *117*, 8497–
672 8520.
- 673 (2) Tomkins, P.; Ranocchiaro, M.; van Bokhoven, J. A. *Acc. Chem.*
674 *Res.* **2017**, *50*, 418–425.
- 675 (3) Horn, R.; Schlögl, R. *Catal. Lett.* **2015**, *145*, 23–39.
- 676 (4) Arutyunov, V. *Catal. Today* **2013**, *215*, 243–250.
- 677 (5) Ravi, M.; Ranocchiaro, M.; van Bokhoven, J. A. *Angew. Chem., Int.*
678 *Ed.* **2017**, *56*, 16464–16483.
- 679 (6) Balasubramanian, R.; Smith, S. M.; Rawat, S.; Yatsunyk, L. A.;
680 Stemmler, T. L.; Rosenzweig, A. C. *Nature* **2010**, *465*, 115–119.
- 681 (7) Groothaert, M. H.; Smeets, P. J.; Sels, B. F.; Jacobs, P. A.;
682 Schoonheydt, R. A. *J. Am. Chem. Soc.* **2005**, *127*, 1394–1395.
- 683 (8) Snyder, B. E. R.; Bols, M. L.; Schoonheydt, R. A.; Sels, B. F.;
684 Solomon, E. I. *Chem. Rev.* **2018**, *118*, 2718–2768.
- 685 (9) Sushkevich, V. L.; Palagin, D.; Ranocchiaro, M.; van Bokhoven, J.
686 *A. Science* **2017**, *356*, 523–527.
- 687 (10) Woertink, J. S.; Smeets, P. J.; Groothaert, M. H.; Vance, M. A.;
688 Sels, B. F.; Schoonheydt, R. A.; Solomon, E. I. *Proc. Natl. Acad. Sci. U.*
689 *S. A.* **2009**, *106*, 18908–18913.
- 690 (11) Alayon, E. M.; Nachtegaal, M.; Ranocchiaro, M.; van Bokhoven,
691 *J. A. Chem. Commun.* **2012**, *48*, 404–406.
- 692 (12) Grundner, S.; Luo, W.; Sanchez-Sanchez, M.; Lercher, J. A.
693 *Chem. Commun.* **2016**, *52*, 2553–2556.
- 694 (13) Grundner, S.; Markovits, M. A.; Li, G.; Tromp, M.; Pidko, E.
695 A.; Hensen, E. J.; Jentys, A.; Sanchez-Sanchez, M.; Lercher, J. A. *Nat.*
696 *Commun.* **2015**, *6*, 7546.
- 697 (14) Tomkins, P.; Mansouri, A.; Bozbag, S. E.; Krumeich, F.; Park,
698 M. B.; Alayon, E. M.; Ranocchiaro, M.; van Bokhoven, J. A. *Angew.*
699 *Chem., Int. Ed.* **2016**, *55*, 5467–5471.
- 700 (15) Wulfers, M. J.; Teketel, S.; Ipek, B.; Lobo, R. F. *Chem. Commun.*
701 **2015**, *51*, 4447–4450.
- 702 (16) Pappas, D. K.; Borfecchia, E.; Dyballa, M.; Pankin, I. A.;
703 Lomachenko, K. A.; Martini, A.; Signorile, M.; Teketel, S.; Arstad, B.;
704 Berlier, G.; Lamberti, C.; Bordiga, S.; Olsbye, U.; Lillerud, K. P.;
705 Svelle, S.; Beato, P. *J. Am. Chem. Soc.* **2017**, *139*, 14961–14975.
- 706 (17) Latimer, A. A.; Kulkarni, A. R.; Aljama, H.; Montoya, J. H.;
707 Yoo, J. S.; Tsai, C.; Abild-Pedersen, F.; Studt, F.; Norskov, J. K. *Nat.*
708 *Mater.* **2017**, *16*, 225–229.
- 709 (18) Palagin, D.; Knorpp, A. J.; Pinar, A. B.; Ranocchiaro, M.; van
710 Bokhoven, J. A. *Nanoscale* **2017**, *9*, 1144–1153.
- 711 (19) Vanelderen, P.; Snyder, B. E.; Tsai, M. L.; Hadt, R. G.;
712 Vancauwenbergh, J.; Coussens, O.; Schoonheydt, R. A.; Sels, B. F.;
713 Solomon, E. I. *J. Am. Chem. Soc.* **2015**, *137*, 6383–6392.
- 714 (20) Alayon, E. M.; Nachtegaal, M.; Bodi, A.; Ranocchiaro, M.; van
715 Bokhoven, J. A. *Phys. Chem. Chem. Phys.* **2015**, *17*, 7681–7693.
- 716 (21) Alayon, E. M. C.; Nachtegaal, M.; Bodi, A.; van Bokhoven, J. A.
717 *ACS Catal.* **2014**, *4*, 16–22.
- 718 (22) Bozbag, S. E.; Alayon, E. M. C.; Pecháček, J.; Nachtegaal, M.;
719 Ranocchiaro, M.; van Bokhoven, J. A. *Catal. Sci. Technol.* **2016**, *6*,
720 5011–5022.
- 721 (23) Snyder, B. E. R.; Vanelderen, P.; Schoonheydt, R. A.; Sels, B. F.;
722 Solomon, E. I. *J. Am. Chem. Soc.* **2018**, *140*, 9236–9243.
- 723 (24) Sushkevich, V. L.; Palagin, D.; van Bokhoven, J. A. *Angew.*
724 *Chem., Int. Ed.* **2018**, *57*, 8906–8910.
- 725 (25) Paolucci, C.; Parekh, A. A.; Khurana, I.; Di Iorio, J. R.; Li, H.;
726 Albarracín Caballero, J. D.; Shih, A. J.; Anggara, T.; Delgass, W. N.;
727 Miller, J. T.; Ribeiro, F. H.; Gounder, R.; Schneider, W. F. *J. Am.*
728 *Chem. Soc.* **2016**, *138*, 6028–6048.
- 729 (26) Paolucci, C.; Khurana, I.; Parekh, A. A.; Li, S. C.; Shih, A. J.; Li,
730 H.; Di Iorio, J. R.; Albarracín-Caballero, J. D.; Yezerets, A.; Miller, J.
731 T.; Delgass, W. N.; Ribeiro, F. H.; Schneider, W. F.; Gounder, R.
732 *Science* **2017**, *357*, 898–903.
- (27) Ravel, B.; Newville, M. J. *Synchrotron Radiat.* **2005**, *12*, 537–
541. 733
- (28) Bellet, D.; Gorges, B.; Dallery, A.; Bernard, P.; Pereira, E.;
Baruchel, J. J. *Appl. Crystallogr.* **2003**, *36*, 366–367. 734
- (29) Giordanino, F.; Borfecchia, E.; Lomachenko, K. A.; Lazzarini,
A.; Agostini, G.; Gallo, E.; Soldatov, A. V.; Beato, P.; Bordiga, S.;
Lamberti, C. *J. Phys. Chem. Lett.* **2014**, *5*, 1552–1559. 735
- (30) Borfecchia, E.; Lomachenko, K. A.; Giordanino, F.; Falsig, H.;
Beato, P.; Soldatov, A. V.; Bordiga, S.; Lamberti, C. *Chem. Sci.* **2015**,
6, 548–563. 736
- (31) Ruckebusch, C. *Resolving Spectral Mixtures: With Applications*
from Ultrafast Time-Resolved Spectroscopy to Super-Resolution Imaging;
Elsevier, 2016; Vol. 30. 737
- (32) de Juan, A.; Tauler, R. *Anal. Chim. Acta* **2003**, *500*, 195–210. 738
- (33) Ruckebusch, C.; Blanchet, L. *Anal. Chim. Acta* **2013**, *765*, 28–
36. 739
- (34) Malinowski, E. R. *Factor Analysis in Chemistry*; Wiley & Sons:
New York, 2002. 740
- (35) Jaumot, J.; Gargallo, R.; de Juan, A.; Tauler, R. *Chemom. Intell.*
Lab. Syst. **2005**, *76*, 101–110. 741
- (36) Windig, W.; Guilment, J. *Anal. Chem.* **1991**, *63*, 1425–1432. 742
- (37) Bro, R.; De Jong, S. J. *Chemom.* **1997**, *11*, 393–401. 743
- (38) Kim, Y.; Kim, T. Y.; Lee, H.; Yi, J. *Chem. Commun.* **2017**, *53*,
4116–4119. 744
- (39) Groothaert, M. H.; van Bokhoven, J. A.; Battiston, A. A.;
Weckhuysen, B. M.; Schoonheydt, R. A. *J. Am. Chem. Soc.* **2003**, *125*,
7629–7640. 745
- (40) Larsen, S. C.; Aylor, A.; Bell, A. T.; Reimer, J. A. *J. Phys. Chem.*
1994, *98*, 11533–11540. 746
- (41) Llabrés i Xamena, F. X.; Fiscaro, P.; Berlier, G.; Zecchina, A.;
Palomino, G. T.; Prestipino, C.; Bordiga, S.; Giamello, E.; Lamberti,
C. *J. Phys. Chem. B* **2003**, *107*, 7036–7044. 747
- (42) Sushkevich, V. L.; van Bokhoven, J. A. *Chem. Commun.* **2018**,
54, 7447–7450. 748
- (43) Martini, A.; Borfecchia, E.; Lomachenko, K. A.; Pankin, I. A.;
Negri, C.; Berlier, G.; Beato, P.; Falsig, H.; Bordiga, S.; Lamberti, C.
Chem. Sci. **2017**, *8*, 6836–6851. 749
- (44) Glatzel, P.; Bergmann, U. *Coord. Chem. Rev.* **2005**, *249*, 65–95. 750
- (45) Singh, J.; Lamberti, C.; van Bokhoven, J. A. *Chem. Soc. Rev.*
2010, *39*, 4754–4766. 751
- (46) Solomon, E. I.; Heppner, D. E.; Johnston, E. M.; Ginsbach, J.
W.; Cirera, J.; Qayyum, M.; Kieber-Emmons, M. T.; Kjaergaard, C.
H.; Hadt, R. G.; Tian, L. *Chem. Rev.* **2014**, *114*, 3659–3853. 752
- (47) Tsai, M. L.; Hadt, R. G.; Vanelderen, P.; Sels, B. F.;
Schoonheydt, R. A.; Solomon, E. I. *J. Am. Chem. Soc.* **2014**, *136*,
3522–3529. 753
- (48) Newton, M. A.; Knorpp, A. J.; Pinar, A. B.; Sushkevich, V. L.;
Palagin, D.; van Bokhoven, J. A. *J. Am. Chem. Soc.* **2018**, *140*, 10090–
10093. 754
- (49) Pidko, E. A.; Hensen, E. J. M.; van Santen, R. A. *Proc. R. Soc.*
London, Ser. A **2012**, *468*, 2070–2086. 755
- (50) Turnes Palomino, G.; Fiscaro, P.; Bordiga, S.; Zecchina, A.;
Giamello, E.; Lamberti, C. *J. Phys. Chem. B* **2000**, *104*, 4064–4073. 756
- (51) Smeets, P. J.; Hadt, R. G.; Woertink, J. S.; Vanelderen, P.;
Schoonheydt, R. A.; Sels, B. F.; Solomon, E. I. *J. Am. Chem. Soc.* **2010**,
132, 14736–14738. 757
- (52) Ipek, B.; Wulfers, M. J.; Kim, H.; Göttl, F.; Hermans, I.; Smith,
J. P.; Booksh, K. S.; Brown, C. M.; Lobo, R. F. *ACS Catal.* **2017**, *7*,
4291–4303. 758